Formulario Liquidi ideali

Liquidi e solidi ideali equazioni di stato
Trasformazione isobara (P = cost) = Trasformazione isocora
- Sistema chiuso $(P_0 = P_1)$
- Sistema aperto stazionario $(P_{in} = P_{out})$
- Liquido ideale
- Scambiatore di calore ideale
- Bilancio entropico sul sottosistema complessivo

Trasformazione isoentropica (s = cost) = Trasformazione isoterma
- Sistema chiuso $(s_0 = s_1)$
- Sistema aperto stazionario $(s_{in} = s_{out})$
- Liquido ideale
- Dispositivo Pompa ideale (compressione isoentropica, TIR)

Fasi → stati della materia
Transizione liquido-vapore
Campana nel diagramma $T - v$
- Campana nei diagrammi $T - s$ e $P - v$
- Tabelle dei valori sulla campana
- Proprietà del liquido saturo e del vapore saturo
- Proprietà del vapore surriscaldato (destra)

Regola della leva
- Titolo di vapore (frazione di gas)
- Frazione di liquido
- Calcolo V → processo analogo anche per H, S, U

Esempi esercizi sui liquidi

Liquidi e solidi ideali equazioni di stato

v → volume specifico è **sempre costante** $[\frac{m^3}{Kg}] = \frac{1}{\rho}$ → il volume non varia mai

c → calore specifico $[\frac{J}{KgK}]$

- c_{H_2O} → 4186 $[\frac{J}{KgK}]$
- ρ_{H_2O} → $1000 \frac{Kg}{m^3}$

L'energia termica che **l'acqua** può **immagazzinare**, rispetto *all'aria*, è enormemente maggiore.

$$\boxed{\begin{matrix} v = \text{costante} \\ \text{Fluido incomprimibile} \end{matrix}} \rightarrow \begin{matrix} \text{Riscaldamento a P costante} \\ = \\ \text{Riscaldamento a V costante} \end{matrix} \rightarrow \boxed{c_p = c_v} = c$$

Non esiste c_v o c_p, ma esiste solamente c → calore specifico

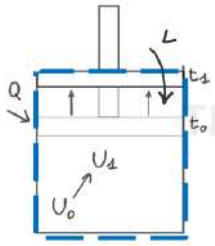
$$\begin{matrix} du = cdT \\ dh = cdT + vdP \\ ds = \frac{c}{T}dT \end{matrix} \quad \begin{matrix} \int_0^1 \\ \longrightarrow \end{matrix} \quad \begin{matrix} u_1 - u_0 = c(T_1 - T_0) \\ h_1 - h_0 = c(T_1 - T_0) + v(P_1 - P_0) \\ s_1 - s_0 = c \ln \frac{T_1}{T_0} \end{matrix}$$

$$dh = d(u + Pv) = du + dPv = du + vdP + \cancel{Pdv} = cdT + vdP$$

📌 La trasformazione **Politropica** è solo e soltanto per il **gas ideale**, non per i **liquidi** o **solidi ideali.**

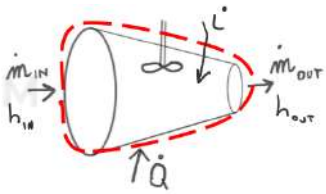
Trasformazione isobara (P = cost) = Trasformazione isocora

Sistema chiuso $(P_0 = P_1)$



$$q_{in} + l_{in} = \Delta u$$
$$l_{in} = -\int Pdv = -P(v_1 - v_0)$$
$$q_{in} = (u_1 + Pv_1) - (u_0 + Pv_o) = \Delta h$$

Sistema aperto stazionario $(P_{in} = P_{out})$



$$q_{in} + l_{in} = \Delta h$$
$$l_{in} = \int vdP = v(\cancel{P_{out} - P_{in}})$$
$$q_{in} = \Delta h$$

1° principio (sistema aperto/chiuso)

$$q_{in} = \Delta h$$

2° principio (sistema aperto/chiuso)

$$\int \frac{\delta q_{in}}{T} = \Delta s$$

$$\boxed{\text{Isobara} + \text{adiabatica} = \text{isoentalpica} \rightarrow \text{iso-h}}$$

$$\Delta h = 0 \rightarrow h_1 = h_0$$

$$\text{in questo caso} \rightarrow \Delta s = 0 \rightarrow \text{adiabatica, no scambi di calore}$$

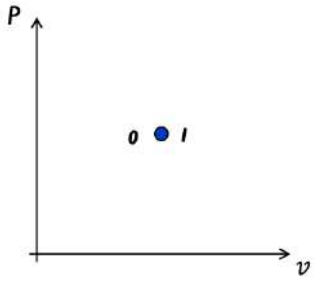
Liquido ideale

Trasformazione isobara = Trasformazione isocora

$$q_{in} = \Delta h =^{\text{Liquido ideale}} c(T_1 - T_0) + v\cancel{(P_1 - P_0)}$$

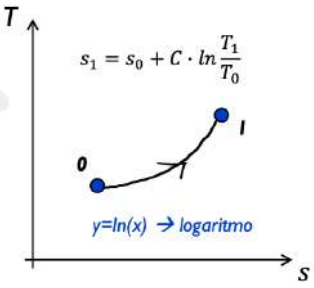
$$\Delta H = Mc\Delta T$$

$$\Delta h = \Delta u$$



Variazione entropia:

$$\Delta s =^{\text{Liquido ideale}} c \cdot \ln \frac{T_1}{T_0}$$

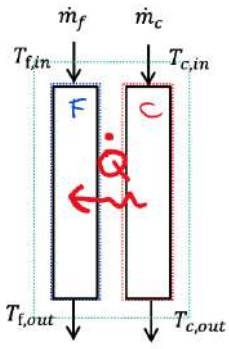


Scambiatore di calore ideale

Costituito da due sistemi **aperti**, quindi è un **sistema aperto**.

(Lo scambiatore, per essere ideale è **TIR** → non ci sono perdite di carico, e anche **adiabatico** → non ci sono dispersioni)

$$\dot{L} = \cancel{\dot{m}v\Delta P} = 0$$



Bilanci su sottosistema freddo: F

1° principio:

$$\dot{Q}_f = \dot{m}_f(h_{f,out} - h_{f,in}) \overset{\text{Liquido ideale}}{=} \dot{m}_f(c(T_{f,out} - T_{f,in}) + v(\cancel{P_{f,out} - P_{f,in}})$$

2° principio:

$$\dot{S}_{Q_f} = \dot{m}_f(s_{f,out} - s_{f,in}) \overset{\text{Liquido ideale}}{=} \dot{m}_f c \ln\left(\frac{T_{f,out}}{T_{f,in}}\right) > 0$$

Bilanci su sottosistema caldo: C

1° principio:

$$-\dot{Q}_c = \dot{m}_c(h_{c,out} - h_{c,in}) \overset{\text{Liquido ideale}}{=} \dot{m}_f(c(T_{c,out} - T_{c,in}) + v(\cancel{P_{c,out} - P_{c,in}})$$

2° principio:

$$\dot{S}_{Q_c} = \dot{m}_c(s_{c,out} - s_{c,in}) \overset{\text{Liquido ideale}}{=} \dot{m}_c c \ln\left(\frac{T_{c,out}}{T_{c,in}}\right) < 0$$

Bilancio entropico sul sottosistema complessivo

$$\dot{S}_{irr} = \Delta\dot{S}_{tot} \rightarrow \dot{S}_{irr} = \dot{m}_f \Delta s_f + \dot{m}_c \Delta s_c \overset{\text{L.I}}{=} \underbrace{\dot{m}_f c \ln\left(\frac{T_{f,out}}{T_{f,in}}\right)}_{>0} + \underbrace{\dot{m}_c c \ln\left(\frac{T_{c,out}}{T_{c,in}}\right)}_{<0} \geq 0$$

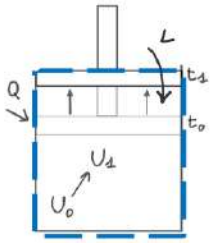
$\dot{S}_{irr}$ è di tipo esterno → c'è uno scambio di calore tra i sottosistemi.

Trasformazione isoentropica (s = cost) = Trasformazione isoterma

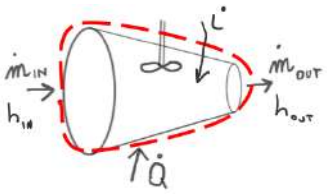
Il **sistema** isoentropico non vuol dire che sia adiabatico. Una **trasformazione** isoentropica è anche adiabatica e viceversa.

Sistema chiuso $(s_0 = s_1)$

Sistema aperto stazionario $(s_{in} = s_{out})$



$$q_{in} + l_{in} = \Delta u$$



$$q_{in} + l_{in} = \Delta h$$

$$q_{in} = \int Tds = T(\cancel{s_1 - s_0}) \quad \boxed{\text{Isoentropica} \rightarrow \text{adiabatica}}$$

$$l_{in} = -\int Pdv = \Delta u$$

1° principio (sistema chiuso)

$$\boxed{l_{in} = \Delta u}$$

$$l_{in} = -\int Pdv = \Delta u$$

1° principio (sistema aperto)

$$\boxed{l_{in} = \Delta h}$$

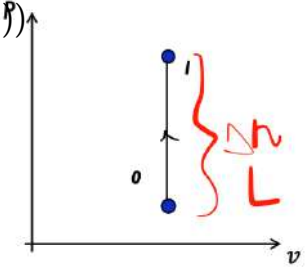
Liquido ideale

Trasformazione **isoentropica** + **Liquido ideale** = Trasformazione **isoterma**

$\dot{L}$ → in termini di potenza $[W]$ → istante per istante

$$\dot{L}_{in} = \dot{m} \int vdP = \dot{m}(h_1 - h_0) = \dot{m}(\cancel{c(T_1 - T_0)} + v(P_1 - P_0))$$

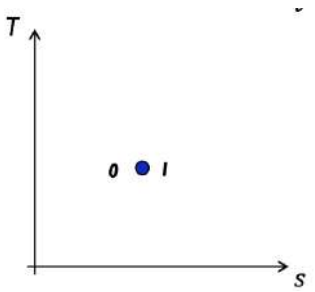
$$\Delta u = 0$$



L'altezza del grafico è proporzionale all'aumento di Δh e quindi di L

Variazione entropia:

$$\cancel{\Delta s} \overset{\text{L.I}}{=} c \cdot \ln \frac{T_1}{T_0} \rightarrow \boxed{T_1 = T_0}$$

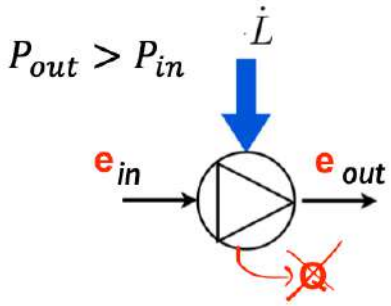


Dispositivo Pompa ideale (compressione isoentropica, TIR)

Essendo la macchina **ideale** è **TIR** → non ci sono attriti ed è **adiabatica** → non ci sono dipersioni.

La **pompa** per il liquido ideale, corrisponde alla **turbina** o **compressore** per il gas ideale.

É un **sistema aperto**.



C'è una compressione, la P aumenta

$$L_{in}^{+} \rightarrow \Delta h^{+}$$

L'energia, essendo un sistema aperto è composta dalla somma di energia interna e del lavoro, la formula è quindi:

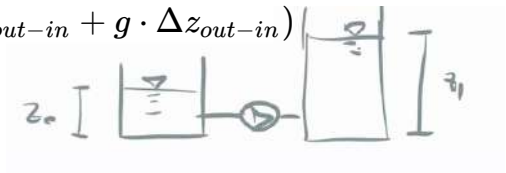
$$e = u + Pv + gz + \frac{1}{2}w^2 \rightarrow \boxed{e = h + gz + \tfrac{1}{2}w^2}$$

Bilancio di 1° principio

$$\dot{L}_{in} = \dot{m}(h_{out} - h_{in}) \overset{\text{L.I, Iso-s}}{=} \dot{m}(v \cdot \Delta P_{out-in})$$

Se la quota potenziale non è trascurabile, allora:

$$\dot{L}_{in} = \dot{m}(h_{out} + gz_{out} - h_{in} - gz_{in}) = \dot{m}(v \cdot \Delta P_{out-in} + g \cdot \Delta z_{out-in})$$



Bilancio di 2° principio

$$\cancel{\dot{S}_{Q_{in}}} - \cancel{\dot{S}_{Q_{out}}} + \cancel{\dot{S}_{irr}} = \dot{m}(s_{out} - s_{in}) \rightarrow \boxed{s_{out} = s_{in}}$$

Fasi → stati della materia

Sostanze **pure** → no mescolamenti

La materia può essere presente in 3 fasi:

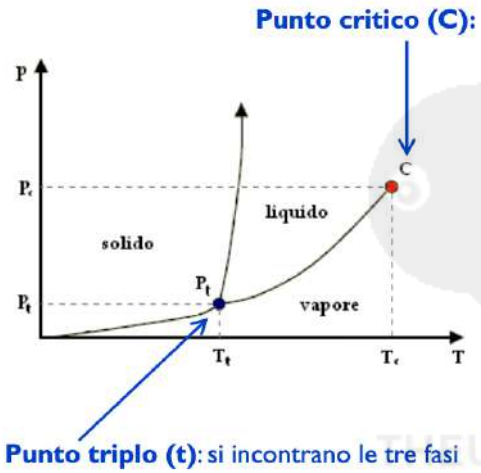
- **Solido**
- **Liquido**
- **Gas - Vapore**

Transizione di fase → passaggio da uno stato all'altro:

- **Solidificazione**: (Liquido → Solido)
- **Fusione**: (Solido → Liquido)
- **Condensazione**: (Gas → Liquido)
- **Evaporazione**: (Liquido → Gas)

Fluidi ideali (modelli semplificati):

- **Gas ideale**: gas a bassa pressione e lontano dalla condensazione.
- **Liquidi / solidi ideali**: lontani dalla transizione di fase.



Punto triplo → si incontrano le tre fasi

Punto triplo acqua $T = 0^\circ C \rightarrow P = 0,006 atm$

Punto critico → Per $T > T_c$: vapore e liquido sono indistinguibili. Non c'è distinzione tra liquido e vapore, dopo di questo si ha il punto super critico

Punto critico acqua → $T = 374^\circ C$ $P = 22 MPa.$

Vapor d'acqua → ~~$Pv = RT$~~ → non è un gas ideale.

Condizioni di **transizione di fase** → **saturazione**.

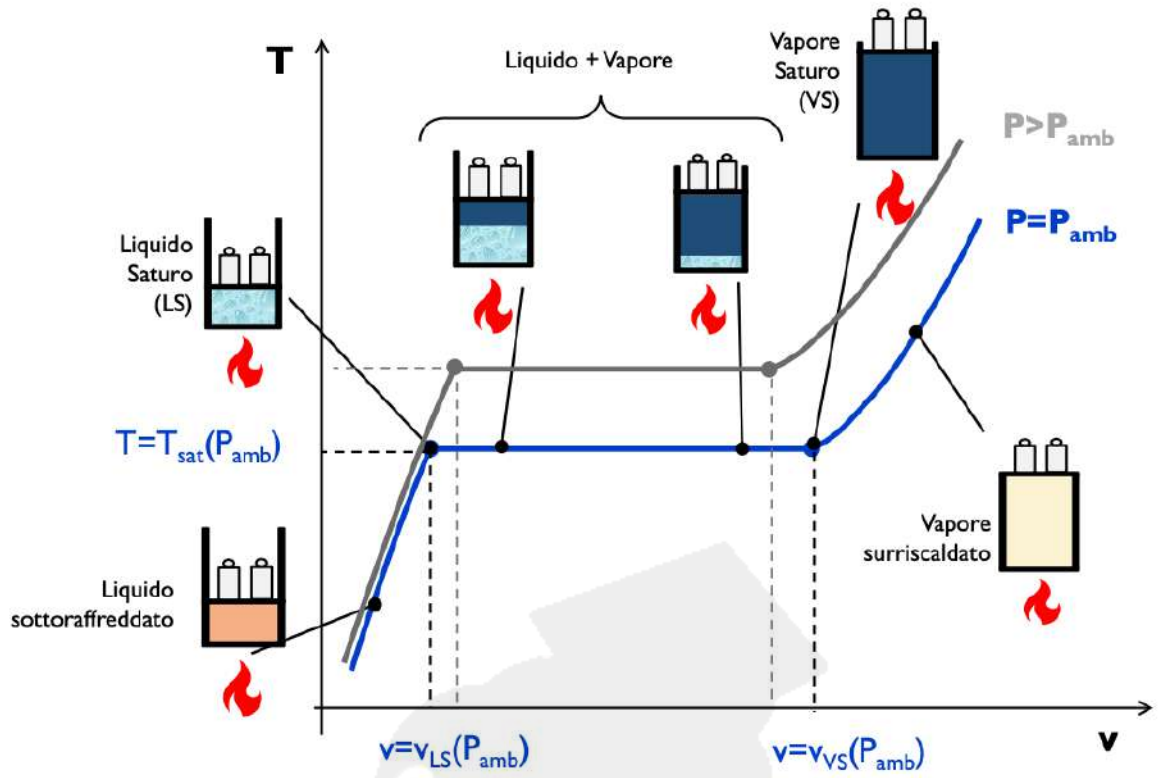
> 📌 L'**acqua è un liquido ideale** se la sua pressione e temperatura sono **minori del punto critico**

Transizione liquido-vapore

Condizioni di transizione di fase → **saturazione**

Quando si raggiunge la temperatura per la transizione di fase, il liquido viene detto **saturo**.

Volume specifico gas >> v liquido → densità ρ gas << densità liquido



pressione > **pressione ambiente**

Es: pentola a pressione, la condizione di saturazione si raggiunge a una temperatura maggiore.

Siccome **varia** il volume specifico → non è un liquido incomprimibile, ma nella realtà è così.

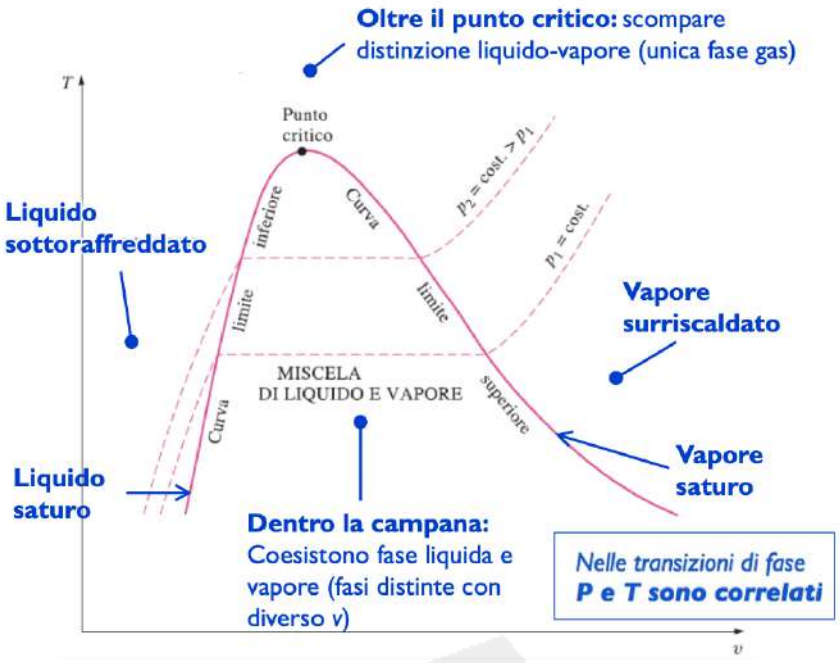
Campana nel diagramma $T - v$

Insieme dei punti di transizione di fase → **luogo dei punti** delle condizioni sature → **campana**

In **condizioni sature**, non possiamo approssimare il liquido a un liquido ideale.

L'apice della campana è la temperatura alle condizioni critiche

Es: acqua → $T = 374,14^{\circ}C$, $P = 22MPa$



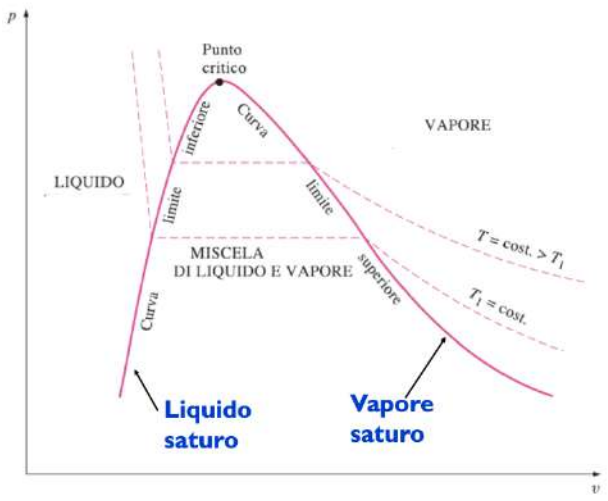
Dentro la campana coesistono liquido e vapore → che sono definite solamente da una proprietà (o temperatura o pressione) → grazie a una delle due possiamo identificare il valore dell'altra → sono legate tra loro. **Isoterma** → utilizziamo la regola della leva con i valori nella tabella

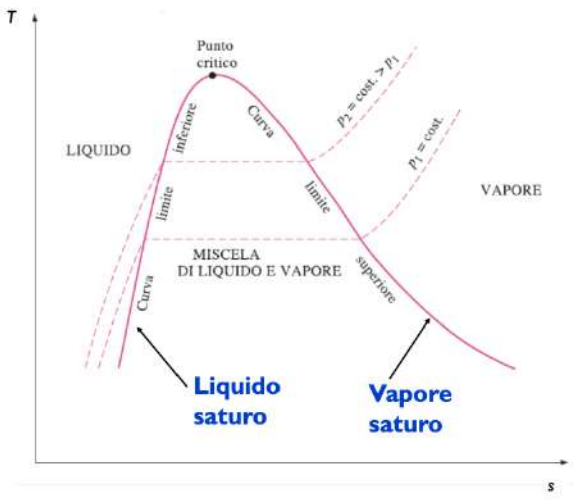
A sinistra della campana → **liquido sotto raffreddato** → definito da due proprietà (T e P) → approssimiamo a liquido ideale (o utilizziamo la tabella)

A destra della campana → **vapore surriscaldato** → definito da due proprietà (T e P) → Utilizziamo la tabella

Campana nei diagrammi $T - s$ e $P - v$

$P - v$→ riscaldamenti e raffreddamenti isotermi → **curve a temperatura costante**





$T - s$ → **curve** a valore **costante di pressione**

Il diagramma $T - s$ sarà quello maggiormente utilizzato.

Tabelle dei valori sulla campana

Proprietà del liquido saturo e del vapore saturo

Valida sulla campana → sulla linea della campana

TABELLA A.4
Acqua satura: tabella in temperatura

Δu Δh Δs

Temp. T °C	Press. sat. p_{sat} kPa	Volume specifico m³/kg: Liquido sat. v_l	Volume specifico m³/kg: Vapore sat. v_v	Energia interna kJ/kg: Liquido sat. u_l	Energia interna kJ/kg: Evap. u_{lv}	Energia interna kJ/kg: Vapore sat. u_v	Entalpia kJ/kg: Liquido sat. h_l	Entalpia kJ/kg: Evap. h_{lv}	Entalpia kJ/kg: Vapore sat. h_v	Entropia kJ/(kg · K): Liquido sat. s_l	Entropia kJ/(kg · K): Evap. s_{lv}	Entropia kJ/(kg · K): Vapore sat. s_v
0.01	0.6113	0.001000	206.14	0.0	2375.3	2375.3	0.01	2501.3	2501.4	0.000	9.1562	9.1562
5	0.8721	0.001000	147.12	20.97	2361.3	2382.3	20.98	2489.6	2510.6	0.0761	8.9496	9.0257
10	1.2276	0.001000	106.38	42.00	2347.2	2389.2	42.01	2477.7	2519.8	0.1510	8.7498	8.9008
15	1.7051	0.001001	77.93	62.99	2333.1	2396.1	62.99	2465.9	2528.9	0.2245	8.5569	8.7814
20	2.339	0.001002	57.79	83.95	2319.0	2402.9	83.96	2454.1	2538.1	0.2966	8.3706	8.6672
25	3.169	0.001003	43.36	104.88	2304.9	2409.8	104.89	2442.3	2547.2	0.3674	8.1905	8.5580
30	4.246	0.001004	32.89	125.78	2290.8	2416.6	125.79	2430.5	2556.3	0.4369	8.0164	8.4533
35	5.628	0.001006	25.22	146.67	2276.7	2423.4	146.68	2418.6	2565.3	0.5053	7.8478	8.3531
40	7.384	0.001008	19.52	167.56	2262.6	2430.1	167.57	2406.7	2574.3	0.5725	7.6845	8.2570
45	9.593	0.001010	15.26	188.44	2248.4	2436.8	188.45	2394.8	2583.2	0.6387	7.5261	8.1648
50	12.349	0.001012	12.03	209.32	2234.2	2443.5	209.33	2382.7	2592.1	0.7038	7.3725	8.0763

▼ Tabella completa in Temperatura

TABELLA A.4
Acqua satura: tabella in temperatura

Temp. T °C	Press. sat. p_{sat} kPa	Volume specifico m³/kg: Liquido sat. v_f	Volume specifico m³/kg: Vapore sat. v_g	Energia interna kJ/kg: Liquido sat. u_f	Energia interna kJ/kg: Evap. u_{fg}	Energia interna kJ/kg: Vapore sat. u_g	Entalpia kJ/kg: Liquido sat. h_f	Entalpia kJ/kg: Evap. h_{fg}	Entalpia kJ/kg: Vapore sat. h_g	Entropia kJ/(kg · K): Liquido sat. s_f	Entropia kJ/(kg · K): Evap. s_{fg}	Entropia kJ/(kg · K): Vapore sat. s_g
0.01	0.6113	0.001000	206.14	0.0	2375.3	2375.3	0.01	2501.3	2501.4	0.000	9.1562	9.1562
5	0.8721	0.001000	147.12	20.97	2361.3	2382.3	20.98	2489.6	2510.6	0.0761	8.9496	9.0257
10	1.2276	0.001000	106.38	42.00	2347.2	2389.2	42.01	2477.7	2519.8	0.1510	8.7498	8.9008
15	1.7051	0.001001	77.93	62.99	2333.1	2396.1	62.99	2465.9	2528.9	0.2245	8.5569	8.7814
20	2.339	0.001002	57.79	83.95	2319.0	2402.9	83.96	2454.1	2538.1	0.2966	8.3706	8.6672
25	3.169	0.001003	43.36	104.88	2304.9	2409.8	104.89	2442.3	2547.2	0.3674	8.1905	8.5580
30	4.246	0.001004	32.89	125.78	2290.8	2416.6	125.79	2430.5	2556.3	0.4369	8.0164	8.4533
35	5.628	0.001006	25.22	146.67	2276.7	2423.4	146.68	2418.6	2565.3	0.5053	7.8478	8.3531
40	7.384	0.001008	19.52	167.56	2262.6	2430.1	167.57	2406.7	2574.3	0.5725	7.6845	8.2570
45	9.593	0.001010	15.26	188.44	2248.4	2436.8	188.45	2394.8	2583.2	0.6387	7.5261	8.1648
50	12.349	0.001012	12.03	209.32	2234.2	2443.5	209.33	2382.7	2592.1	0.7038	7.3725	8.0763
55	15.758	0.001015	9.568	230.21	2219.9	2450.1	230.23	2370.7	2600.9	0.7679	7.2234	7.9913
60	19.940	0.001017	7.671	251.11	2205.5	2456.6	251.13	2358.5	2609.6	0.8312	7.0784	7.9096
65	25.03	0.001020	6.197	272.02	2191.1	2463.1	272.06	2346.2	2618.3	0.8935	6.9375	7.8310
70	31.19	0.001023	5.042	292.95	2176.6	2469.6	292.98	2333.8	2626.8	0.9549	6.8004	7.7553
75	38.58	0.001026	4.131	313.90	2162.0	2475.9	313.93	2321.4	2635.3	1.0155	6.6669	7.6824
80	47.39	0.001029	3.407	334.86	2147.4	2482.2	334.91	2308.8	2643.7	1.0753	6.5369	7.6122
85	57.83	0.001033	2.828	355.84	2132.6	2488.4	355.90	2296.0	2651.9	1.1343	6.4102	7.5445
90	70.14	0.001036	2.361	376.85	2117.7	2494.5	376.92	2283.2	2660.1	1.1925	6.2866	7.4791
95	84.55	0.001040	1.982	397.88	2102.7	2500.6	397.96	2270.2	2668.1	1.2500	6.1659	7.4159
	Press. sat. MPa											
100	0.10133	0.001044	1.6729	418.94	2087.6	2506.5	419.04	2257.0	2676.1	1.3069	6.0480	7.3549
105	0.12082	0.001048	1.4194	440.02	2072.3	2512.4	440.15	2243.7	2683.8	1.3630	5.9328	7.2958
110	0.14327	0.001052	1.2102	461.14	2057.0	2518.1	461.30	2230.2	2691.5	1.4185	5.8202	7.2387
115	0.16906	0.001056	1.0366	482.30	2041.4	2523.7	482.48	2216.5	2699.0	1.4734	5.7100	7.1833
120	0.19853	0.001060	0.8919	503.50	2025.8	2529.3	503.71	2202.6	2706.3	1.5276	5.6020	7.1296
125	0.2321	0.001065	0.7706	524.74	2009.9	2534.6	524.99	2188.5	2713.5	1.5813	5.4962	7.0775
130	0.2701	0.001070	0.6685	546.02	1993.9	2539.9	546.31	2174.2	2720.5	1.6344	5.3925	7.0269
135	0.3130	0.001075	0.5822	567.35	1977.7	2545.0	567.69	2159.6	2727.3	1.6870	5.2907	6.9777
140	0.3613	0.001080	0.5089	588.74	1961.3	2550.0	589.13	2144.7	2733.9	1.7391	5.1908	6.9299
145	0.4154	0.001085	0.4463	610.18	1944.7	2554.9	610.63	2129.6	2740.3	1.7907	5.0926	6.8833
150	0.4758	0.001091	0.3928	631.68	1927.9	2559.5	632.20	2114.3	2746.5	1.8418	4.9960	6.8379
155	0.5431	0.001096	0.3468	653.24	1910.8	2564.1	653.84	2098.6	2752.4	1.8925	4.9010	6.7935
160	0.6178	0.001102	0.3071	674.87	1893.5	2568.4	675.55	2082.6	2758.1	1.9427	4.8075	6.7502
165	0.7005	0.001108	0.2727	696.56	1876.0	2572.5	697.34	2066.2	2763.5	1.9925	4.7153	6.7078
170	0.7917	0.001114	0.2428	718.33	1858.1	2576.5	719.21	2049.5	2768.7	2.0419	4.6244	6.6663
175	0.8920	0.001121	0.2168	740.17	1840.0	2580.2	741.17	2032.4	2773.6	2.0909	4.5347	6.6256
180	1.0021	0.001127	0.19405	762.09	1821.6	2583.7	763.22	2015.0	2778.2	2.1396	4.4461	6.5857
185	1.1227	0.001134	0.17409	784.10	1802.9	2587.0	785.37	1997.1	2782.4	2.1879	4.3586	6.5465
190	1.2544	0.001141	0.15654	806.19	1783.8	2590.0	807.62	1978.8	2786.4	2.2359	4.2720	6.5079
195	1.3978	0.001149	0.14105	828.37	1764.4	2592.8	829.98	1960.0	2790.0	2.2835	4.1863	6.4698

TABELLA A.4

Acqua satura: tabella in temperatura (*continua*)

Temp. T °C	Press. sat. p_{sat} MPa	Volume specifico m³/kg: Liquido sat. v_l	Volume specifico m³/kg: Vapore sat. v_v	Energia interna kJ/kg: Liquido sat. u_l	Energia interna kJ/kg: Evap. u_{lv}	Energia interna kJ/kg: Vapore sat. u_v	Entalpia kJ/kg: Liquido sat. h_l	Entalpia kJ/kg: Evap. h_{lv}	Entalpia kJ/kg: Vapore sat. h_v	Entropia kJ/(kg · K): Liquido sat. s_l	Entropia kJ/(kg · K): Evap. s_{lv}	Entropia kJ/(kg · K): Vapore sat. s_v
200	1.5538	0.001157	0.12736	850.65	1744.7	2595.3	852.45	1940.7	2793.2	2.3309	4.1014	6.4323
205	1.7230	0.001164	0.11521	873.04	1724.5	2597.5	875.04	1921.0	2796.0	2.3780	4.0172	6.3952
210	1.9062	0.001173	0.10441	895.53	1703.9	2599.5	897.76	1900.7	2798.5	2.4248	3.9337	6.3585
215	2.104	0.001181	0.09479	918.14	1682.9	2601.1	920.62	1879.9	2800.5	2.4714	3.8507	6.3221
220	2.318	0.001190	0.08619	940.87	1661.5	2602.4	943.62	1858.5	2802.1	2.5178	3.7683	6.2861
225	2.548	0.001199	0.07849	963.73	1639.6	2603.3	966.78	1836.5	2803.3	2.5639	3.6863	6.2503
230	2.795	0.001209	0.07158	986.74	1617.2	2603.9	990.12	1813.8	2804.0	2.6099	3.6047	6.2146
235	3.060	0.001219	0.06537	1009.89	1594.2	2604.1	1013.62	1790.5	2804.2	2.6558	3.5233	6.1791
240	3.344	0.001229	0.05976	1033.21	1570.8	2604.0	1037.32	1766.5	2803.8	2.7015	3.4422	6.1437
245	3.648	0.001240	0.05471	1056.71	1546.7	2603.4	1061.23	1741.7	2803.0	2.7472	3.3612	6.1083
250	3.973	0.001251	0.05013	1080.39	1522.0	2602.4	1085.36	1716.2	2801.5	2.7927	3.2802	6.0730
255	4.319	0.001263	0.04598	1104.28	1596.7	2600.9	1109.73	1689.8	2799.5	2.8383	3.1992	6.0375
260	4.688	0.001276	0.04221	1128.39	1470.6	2599.0	1134.37	1662.5	2796.9	2.8838	3.1181	6.0019
265	5.081	0.001289	0.03877	1152.74	1443.9	2596.6	1159.28	1634.4	2793.6	2.9294	3.0368	5.9662
270	5.499	0.001302	0.03564	1177.36	1416.3	2593.7	1184.51	1605.2	2789.7	2.9751	2.9551	5.9301
275	5.942	0.001317	0.03279	1202.25	1387.9	2590.2	1210.07	1574.9	2785.0	3.0208	2.8730	5.8938
280	6.412	0.001332	0.03017	1227.46	1358.7	2586.1	1235.99	1543.6	2779.6	3.0668	2.7903	5.8571
285	6.909	0.001348	0.02777	1253.00	1328.4	2581.4	1262.31	1511.0	2773.3	3.1130	2.7070	5.8199
290	7.436	0.001366	0.02557	1278.92	1297.1	2576.0	1289.07	1477.1	2766.2	3.1594	2.6227	5.7821
295	7.993	0.001384	0.02354	1305.2	1264.7	2569.9	1316.3	1441.8	2758.1	3.2062	2.5375	5.7437
300	8.581	0.001404	0.02167	1332.0	1231.0	2563.0	1344.0	1404.9	2749.0	3.2534	2.4511	5.7045
305	9.202	0.001425	0.019948	1359.3	1195.9	2555.2	1372.4	1366.4	2738.7	3.3010	2.3633	5.6643
310	9.856	0.001447	0.018350	1387.1	1159.4	2546.4	1401.3	1326.0	2727.3	3.3493	2.2737	5.6230
315	10.547	0.001472	0.016867	1415.5	1121.1	2536.6	1431.0	1283.5	2714.5	3.3982	2.1821	5.5804
320	11.274	0.001499	0.015488	1444.6	1080.9	2525.5	1461.5	1238.6	2700.1	3.4480	2.0882	5.5362
330	12.845	0.001561	0.012996	1505.3	993.7	2498.9	1525.3	1140.6	2665.9	3.5507	1.8909	5.4417
340	14.586	0.001638	0.010797	1570.3	894.3	2464.6	1594.2	1027.9	2622.0	3.6594	1.6763	5.3357
350	16.513	0.001740	0.008813	1641.9	776.6	2418.4	1670.6	893.4	2563.9	3.7777	1.4335	5.2112
360	18.651	0.001893	0.006945	1725.2	626.3	2351.5	1760.5	720.3	2481.0	3.9147	1.1379	5.0526
370	21.03	0.002213	0.004925	1844.0	384.5	2228.5	1890.5	441.6	2332.1	4.1106	0.6865	4.7971
374.14	22.09	0.003155	0.003155	2029.6	0	2029.6	2099.3	0	2099.3	4.4298	0	4.4298

Fonte per le tabelle da A.4 fino ad A.6: J.H. Keenan, F.G. Keyes, P.G. Hill e J.G. Moore, *Steam Tables*, SI Units, Wiley, New York 1978.

▼ Tabella completa in Pressione

TABELLA A.5
Acqua satura: tabella in pressione

Press. p kPa	Temp. sat. T_{sat} °C	Volume specifico m³/kg		Energia interna kJ/kg			Entalpia kJ/kg			Entropia kJ/(kg · K)		
		Liquido sat. v_f	Vapore sat. v_g	Liquido sat. u_f	Evap. u_{fg}	Vapore sat. u_g	Liquido sat. h_f	Evap. h_{fg}	Vapore sat. h_g	Liquido sat. s_f	Evap. s_{fg}	Vapore sat. s_g
0.6113	0.01	0.001000	206.14	0.00	2375.3	2375.3	0.01	2501.3	2501.4	0.0000	9.1562	9.1562
1.0	6.98	0.001000	129.21	29.30	2355.7	2385.0	29.30	2484.9	2514.2	0.1059	8.8697	8.9756
1.5	13.03	0.001001	87.98	54.71	2338.6	2393.3	54.71	2470.6	2525.3	0.1957	8.6322	8.8279
2.0	17.50	0.001001	67.00	73.48	2326.0	2399.5	73.48	2460.0	2533.5	0.2607	8.4629	8.7237
2.5	21.08	0.001002	54.25	88.48	2315.9	2404.4	88.49	2451.6	2540.0	0.3120	8.3311	8.6432
3.0	24.08	0.001003	45.67	101.04	2307.5	2408.5	101.05	2444.5	2545.5	0.3545	8.2231	8.5776
4.0	28.96	0.001004	34.80	121.45	2293.7	2415.2	121.46	2432.9	2554.4	0.4226	8.0520	8.4746
5.0	32.88	0.001005	28.19	137.81	2282.7	2420.5	137.82	2423.7	2561.5	0.4764	7.9187	8.3951
7.5	40.29	0.001008	19.24	168.78	2261.7	2430.5	168.79	2406.0	2574.8	0.5764	7.6750	8.2515
10	45.81	0.001010	14.67	191.82	2246.1	2437.9	191.83	2392.8	2584.7	0.6493	7.5009	8.1502
15	53.97	0.001014	10.02	225.92	2222.8	2448.7	225.94	2373.1	2599.1	0.7549	7.2536	8.0085
20	60.06	0.001017	7.649	251.38	2205.4	2456.7	251.40	2358.3	2609.7	0.8320	7.0766	7.9085
25	64.97	0.001020	6.204	271.90	2191.2	2463.1	271.93	2346.3	2618.2	0.8931	6.9383	7.8314
30	69.10	0.001022	5.229	289.20	2179.2	2468.4	289.23	2336.1	2625.3	0.9439	6.8247	7.7686
40	75.87	0.001027	3.993	317.53	2159.5	2477.0	317.58	2319.2	2636.8	1.0259	6.6441	7.6700
50	81.33	0.001030	3.240	340.44	2143.4	2483.9	340.49	2305.4	2645.9	1.0910	6.5029	7.5939
75	91.78	0.001037	2.217	384.31	2112.4	2496.7	384.39	2278.6	2663.0	1.2130	6.2434	7.4564
Press. MPa												
0.100	99.63	0.001043	1.6940	417.36	2088.7	2506.1	417.46	2258.0	2675.5	1.3026	6.0568	7.3594
0.125	105.99	0.001048	1.3749	444.19	2069.3	2513.5	444.32	2241.0	2685.4	1.3740	5.9104	7.2844
0.150	111.37	0.001053	1.1593	466.94	2052.7	2519.7	467.11	2226.5	2693.6	1.4336	5.7897	7.2233
0.175	116.06	0.001057	1.0036	486.80	2038.1	2524.9	486.99	2213.6	2700.6	1.4849	5.6868	7.1717
0.200	120.23	0.001061	0.8857	504.49	2025.0	2529.5	504.70	2201.9	2706.7	1.5301	5.5970	7.1271
0.225	124.00	0.001064	0.7933	520.47	2013.1	2533.6	520.72	2191.3	2712.1	1.5706	5.5173	7.0878
0.250	127.44	0.001067	0.7187	535.10	2002.1	2537.2	535.37	2181.5	2716.9	1.6072	5.4455	7.0527
0.275	130.60	0.001070	0.6573	548.59	1991.9	2540.5	548.89	2172.4	2721.3	1.6408	5.3801	7.0209
0.300	133.55	0.001073	0.6058	561.15	1982.4	2543.6	561.47	2163.8	2725.3	1.6718	5.3201	6.9919
0.325	136.30	0.001076	0.5620	572.90	1973.5	2546.4	573.25	2155.8	2729.0	1.7006	5.2646	6.9652
0.350	138.88	0.001079	0.5243	583.95	1965.0	2548.9	584.33	2148.1	2732.4	1.7275	5.2130	6.9405
0.375	141.32	0.001081	0.4914	594.40	1956.9	2551.3	594.81	2140.8	2735.6	1.7528	5.1647	6.9175
0.40	143.63	0.001084	0.4625	604.31	1949.3	2553.6	604.74	2133.8	2738.6	1.7766	5.1193	6.8959
0.45	147.93	0.001088	0.4140	622.77	1934.9	2557.6	623.25	2120.7	2743.9	1.8207	5.0359	6.8565
0.50	151.86	0.001093	0.3749	639.68	1921.6	2561.2	640.23	2108.5	2748.7	1.8607	4.9606	6.8213
0.55	155.48	0.001097	0.3427	655.32	1909.2	2564.5	665.93	2097.0	2753.0	1.8973	4.8920	6.7893
0.60	158.85	0.001101	0.3157	669.90	1897.5	2567.4	670.56	2086.3	2756.8	1.9312	4.8288	6.7600
0.65	162.01	0.001104	0.2927	683.56	1886.5	2570.1	684.28	2076.0	2760.3	1.9627	4.7703	6.7331
0.70	164.97	0.001108	0.2729	696.44	1876.1	2572.5	697.22	2066.3	2763.5	1.9922	4.7158	6.7080
0.75	167.78	0.001112	0.2556	708.64	1866.1	2574.7	709.47	2057.0	2766.4	2.0200	4.6647	6.6847
0.80	170.43	0.001115	0.2404	720.22	1856.6	2576.8	721.11	2048.0	2769.1	2.0462	4.6166	6.6628
0.85	172.96	0.001118	0.2270	731.27	1847.4	2578.7	732.22	2039.4	2771.6	2.0710	4.5711	6.6421
0.90	175.38	0.001121	0.2150	741.83	1838.6	2580.5	742.83	2031.1	2773.9	2.0946	4.5280	6.6226
0.95	177.69	0.001124	0.2042	751.95	1830.2	2582.1	753.02	2023.1	2776.1	2.1172	4.4869	6.6041
1.00	179.91	0.001127	0.19444	761.68	1822.0	2583.6	762.81	2015.3	2778.1	2.1387	4.4478	6.5865
1.10	184.09	0.001133	0.17753	780.09	1806.3	2586.4	781.34	2000.4	2781.7	2.1792	4.3744	6.5536
1.20	187.99	0.001139	0.16333	797.29	1791.5	2588.8	798.65	1986.2	2784.8	2.2166	4.3067	6.5233
1.30	191.64	0.001144	0.15125	813.44	1777.5	2591.0	814.93	1972.7	2787.6	2.2515	4.2438	6.4953

TABELLA A.5
Acqua satura: tabella in pressione (*continua*)

Press. p MPa	Temp. sat. T_{sat} °C	Volume specifico m³/kg: Liquido sat. v_f	Volume specifico m³/kg: Vapore sat. v_g	Energia interna kJ/kg: Liquido sat. u_f	Energia interna kJ/kg: Evap. u_{fg}	Energia interna kJ/kg: Vapore sat. u_g	Entalpia kJ/kg: Liquido sat. h_f	Entalpia kJ/kg: Evap. h_{fg}	Entalpia kJ/kg: Vapore sat. h_g	Entropia kJ/(kg · K): Liquido sat. s_f	Entropia kJ/(kg · K): Evap. s_{fg}	Entropia kJ/(kg · K): Vapore sat. s_g
1.40	195.07	0.001149	0.14084	828.70	1764.1	2592.8	830.30	1959.7	2790.0	2.2842	4.1850	6.4693
1.50	198.32	0.001154	0.13177	843.16	1751.3	2594.5	844.89	1947.3	2792.2	2.3150	4.1298	6.4448
1.75	205.76	0.001166	0.11349	876.46	1721.4	2597.8	878.50	1917.9	2796.4	2.3851	4.0044	6.3896
2.00	212.42	0.001177	0.09963	906.44	1693.8	2600.3	908.79	1890.7	2799.5	2.4474	3.8935	6.3409
2.25	218.45	0.001187	0.08875	933.83	1668.2	2602.0	936.49	1865.2	2801.7	2.5035	3.7937	6.2972
2.5	223.99	0.001197	0.07998	959.11	1644.0	2603.1	962.11	1841.0	2803.1	2.5547	3.7028	6.2575
3.0	233.90	0.001217	0.06668	1004.78	1599.3	2604.1	1008.42	1795.7	2804.2	2.6457	3.5412	6.1869
3.5	242.60	0.001235	0.05707	1045.43	1558.3	2603.7	1049.75	1753.7	2803.4	2.7253	3.4000	6.1253
4	250.40	0.001252	0.04978	1082.31	1520.0	2602.3	1087.31	1714.1	2801.4	2.7964	3.2737	6.0701
5	263.99	0.001286	0.03944	1147.81	1449.3	2597.1	1154.23	1640.1	2794.3	2.9202	3.0532	5.9734
6	275.64	0.001319	0.03244	1205.44	1384.3	2589.7	1213.35	1571.0	2784.3	3.0267	2.8625	5.8892
7	285.88	0.001351	0.027437	1257.55	1323.0	2580.5	1267.00	1505.1	2772.1	3.1211	2.6922	5.8133
8	295.06	0.001384	0.02352	1305.57	1264.2	2569.8	1316.64	1441.3	2758.0	3.2068	2.5364	5.7432
9	303.40	0.001418	0.02048	1350.51	1207.3	2557.8	1363.26	1378.9	2742.1	3.2858	2.3915	5.6722
10	311.06	0.001452	0.018026	1393.04	1151.4	2544.4	1407.56	1317.1	2724.7	3.3596	2.2544	5.6141
11	318.15	0.001489	0.015987	1433.7	1096.0	2529.8	1450.1	1255.5	2705.6	3.4295	2.1233	5.5527
12	324.75	0.001527	0.014263	1473.0	1040.7	2513.7	1491.3	1193.3	2684.9	3.4962	1.9962	5.4924
13	330.93	0.001567	0.012780	1511.1	985.0	2496.1	1531.5	1130.7	2662.2	3.5606	1.8718	5.4323
14	336.75	0.001611	0.011485	1548.6	928.2	2476.8	1571.1	1066.5	2637.6	3.6232	1.7485	5.3717
15	342.24	0.001658	0.010337	1585.6	869.8	2455.5	1610.5	1000.0	2610.5	3.6848	1.6249	5.3098
16	347.44	0.001711	0.009306	1622.7	809.0	2431.7	1650.1	930.6	2580.6	3.7461	1.4994	5.2455
17	352.37	0.001770	0.008364	1660.2	744.8	2405.0	1690.3	856.9	2547.2	3.8079	1.3698	5.1777
18	357.06	0.001840	0.007489	1698.9	675.4	2374.3	1732.0	777.1	2509.1	3.8715	1.2329	5.1044
19	361.54	0.001924	0.006657	1739.9	598.1	2338.1	1776.5	688.0	2464.5	3.9388	1.0839	5.0228
20	365.81	0.002036	0.005834	1785.6	507.5	2293.0	1826.3	583.4	2409.7	4.0139	0.9130	4.9269
21	369.89	0.002207	0.004952	1842.1	388.5	2230.6	1888.4	446.2	2334.6	4.1075	0.6938	4.8013
22	373.80	0.002742	0.003568	1961.9	125.2	2087.1	2022.2	143.4	2165.6	4.3110	0.2216	4.5327
22.09	374.14	0.003155	0.003155	2029.6	0	2029.6	2099.3	0	2099.3	4.4298	0	4.4298

In **condizioni sature**, non possiamo approssimare il liquido a un liquido ideale.

L'apice della campana è la temperatura alle condizioni critiche → 374,14°C

Proprietà del vapore surriscaldato (destra)

Tabella A.6 → fuori dalla campana, a destra

TABELLA A.6
Acqua surriscaldata

T °C	volume specifico m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)	volume specifico m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)	volume specifico m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)
	p = 0.01 MPa (45.81°C)*				p = 0.05 MPa (81.33°C)				p = 0.10 MPa (99.63°C)			
Sat.†	14.674	2437.9	2584.7	8.1502	3.240	2483.9	2645.9	7.5939	1.6940	2506.1	2675.5	7.3594
50	14.869	2443.9	2592.6	8.1749								
100	17.196	2515.5	2687.5	8.4479	3.418	2511.6	2682.5	7.6947	1.6958	2506.7	2676.2	7.3614
150	19.512	2587.9	2783.0	8.6882	3.889	2585.6	2780.1	7.9401	1.9364	2582.8	2776.4	7.6134
200	21.825	2661.3	2879.5	8.9038	4.356	2659.9	2877.7	8.1580	2.172	2658.1	2875.3	7.8343
250	24.136	2736.0	2977.3	9.1002	4.820	2735.0	2976.0	8.3556	2.406	2733.7	2974.3	8.0333
300	26.445	2812.1	3076.5	9.2813	5.284	2811.3	3075.5	8.5373	2.639	2810.4	3074.3	8.2158
400	31.063	2968.9	3279.6	9.6077	6.209	2968.5	3278.9	8.8642	3.103	2967.9	3278.2	8.5435
500	35.679	3132.3	3489.1	9.8978	7.134	3132.0	3488.7	9.1546	3.565	3131.6	3488.1	8.8342
600	40.295	3302.5	3705.4	10.1608	8.057	3302.2	3705.1	9.4178	4.028	3301.9	3704.4	9.0976
700	44.911	3479.6	3928.7	10.4028	8.981	3479.4	3928.5	9.6599	4.490	3479.2	3928.2	9.3398
800	49.526	3663.8	4159.0	10.6281	9.904	3663.6	4158.9	9.8852	4.952	3663.5	4158.6	9.5652

▼ Tabella completa

TABELLA A.6
Acqua surriscaldata

T °C	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)
	p = 0.01 MPa (45.81°C)*				p = 0.05 MPa (81.33°C)				p = 0.10 MPa (99.63°C)			
Sat.†	14.674	2437.9	2584.7	8.1502	3.240	2483.9	2645.9	7.5939	1.6940	2506.1	2675.5	7.3594
50	14.869	2443.9	2592.6	8.1749								
100	17.196	2515.5	2687.5	8.4479	3.418	2511.6	2682.5	7.6947	1.6958	2506.7	2676.2	7.3614
150	19.512	2587.9	2783.0	8.6882	3.889	2585.6	2780.1	7.9401	1.9364	2582.8	2776.4	7.6134
200	21.825	2661.3	2879.5	8.9038	4.356	2659.9	2877.7	8.1580	2.172	2658.1	2875.3	7.8343
250	24.136	2736.0	2977.3	9.1002	4.820	2735.0	2976.0	8.3556	2.406	2733.7	2974.3	8.0333
300	26.445	2812.1	3076.5	9.2813	5.284	2811.3	3075.5	8.5373	2.639	2810.4	3074.3	8.2158
400	31.063	2968.9	3279.6	9.6077	6.209	2968.5	3278.9	8.8642	3.103	2967.9	3278.2	8.5435
500	35.679	3132.3	3489.1	9.8978	7.134	3132.0	3488.7	9.1546	3.565	3131.6	3488.1	8.8342
600	40.295	3302.5	3705.4	10.1608	8.057	3302.2	3705.1	9.4178	4.028	3301.9	3704.4	9.0976
700	44.911	3479.6	3928.7	10.4028	8.981	3479.4	3928.5	9.6599	4.490	3479.2	3928.2	9.3398
800	49.526	3663.8	4159.0	10.6281	9.904	3663.6	4158.9	9.8852	4.952	3663.5	4158.6	9.5652
900	54.141	3855.0	4396.4	10.8396	10.828	3854.9	4396.3	10.0967	5.414	3854.8	4396.1	9.7767
1000	58.757	4053.0	4640.6	11.0393	11.751	4052.9	4640.5	10.2964	5.875	4052.8	4640.3	9.9764
1100	63.372	4257.5	4891.2	11.2287	12.674	4257.4	4891.1	10.4859	6.337	4257.3	4891.0	10.1659
1200	67.987	4467.9	5147.8	11.4091	13.597	4467.8	5147.7	10.6662	6.799	4467.7	5147.6	10.3463
1300	72.602	4683.7	5409.7	11.5811	14.521	4683.6	5409.6	10.8382	7.260	4683.5	5409.5	10.5183
	p = 0.20 MPa (120.23°C)				p = 0.30 MPa (133.55°C)				p = 0.40 MPa (143.63°C)			
Sat.	0.8857	2529.5	2706.7	7.1272	0.6058	2543.6	2725.3	6.9919	0.4625	2553.6	2738.6	6.8959
150	0.9596	2576.9	2768.8	7.2795	0.6339	2570.8	2761.0	7.0778	0.4708	2564.5	2752.8	6.9299
200	1.0803	2654.4	2870.5	7.5066	0.7163	2650.7	2865.6	7.3115	0.5342	2646.8	2860.5	7.1706
250	1.1988	2731.2	2971.0	7.7086	0.7964	2728.7	2967.6	7.5166	0.5951	2726.1	2964.2	7.3789
300	1.3162	2808.6	3071.8	7.8926	0.8753	2806.7	3069.3	7.7022	0.6548	2804.8	3066.8	7.5662
400	1.5493	2966.7	3276.6	8.2218	1.0315	2965.6	3275.0	8.0330	0.7726	2964.4	3273.4	7.8985
500	1.7814	3130.8	3487.1	8.5133	1.1867	3130.0	3486.0	8.3251	0.8893	3129.2	3484.9	8.1913
600	2.013	3301.4	3704.0	8.7770	1.3414	3300.8	3703.2	8.5892	1.0055	3300.2	3702.4	8.4558
700	2.244	3478.8	3927.6	9.0194	1.4957	3478.4	3927.1	8.8319	1.1215	3477.9	3926.5	8.6987
800	2.475	3663.1	4158.2	9.2449	1.6499	3662.9	4157.8	9.0576	1.2372	3662.4	4157.3	8.9244
900	2.705	3854.5	4395.8	9.4566	1.8041	3854.2	4395.4	9.2692	1.3529	3853.9	4395.1	9.1362
1000	2.937	4052.5	4640.0	9.6563	1.9581	4052.3	4639.7	9.4690	1.4685	4052.0	4639.4	9.3360
1100	3.168	4257.0	4890.7	9.8458	2.1121	4256.8	4890.4	9.6585	1.5840	4256.5	4890.2	9.5256
1200	3.399	4467.5	5147.5	10.0262	2.2661	4467.2	5147.1	9.8389	1.6996	4467.0	5146.8	9.7060
1300	3.630	4683.2	5409.3	10.1982	2.4201	4683.0	5409.0	10.0110	1.8151	4682.8	5408.8	9.8780
	p = 0.50 MPa (151.86°C)				p = 0.60 MPa (158.85°C)				p = 0.80 MPa (170.43°C)			
Sat.	0.3749	2561.2	2748.7	6.8213	0.3157	2567.4	2756.8	6.7600	0.2404	2576.8	2769.1	6.6628
200	0.4249	2642.9	2855.4	7.0592	0.3520	2638.9	2850.1	6.9665	0.2608	2630.6	2839.3	6.8158
250	0.4744	2723.5	2960.7	7.2709	0.3938	2720.9	2957.2	7.1816	0.2931	2715.5	2950.0	7.0384
300	0.5226	2802.9	3064.2	7.4599	0.4344	2801.0	3061.6	7.3724	0.3241	2797.2	3056.5	7.2328
350	0.5701	2882.6	3167.7	7.6329	0.4742	2881.2	3165.7	7.5464	0.3544	2878.2	3161.7	7.4089
400	0.6173	2963.2	3271.9	7.7938	0.5137	2962.1	3270.3	7.7079	0.3843	2959.7	3267.1	7.5716
500	0.7109	3128.4	3483.9	8.0873	0.5920	3127.6	3482.8	8.0021	0.4433	3126.0	3480.6	7.8673
600	0.8041	3299.6	3701.7	7.3522	0.6697	3299.1	3700.9	8.2674	0.5018	3297.9	3699.4	8.1333
700	0.8969	3477.5	3925.9	8.5952	0.7472	3477.0	3925.3	8.5107	0.5601	3476.2	3924.2	8.3770
800	0.9896	3662.1	4156.9	8.8211	0.8245	3661.8	4156.5	8.7367	0.6181	3661.1	4155.6	8.6033
900	1.0822	3853.6	4394.7	9.0329	0.9017	3853.4	4394.4	8.9486	0.6761	3852.8	4393.7	8.8153
1000	1.1747	4051.8	4639.1	9.2328	0.9788	4051.5	4638.8	9.1485	0.7340	4051.0	4638.2	9.0153
1100	1.2672	4256.3	4889.9	9.4224	1.0559	4256.1	4889.6	9.3381	0.7919	4255.6	4889.1	9.2050
1200	1.3596	4466.8	5146.6	9.6029	1.1330	4466.5	5146.3	9.5185	0.8497	4466.1	5145.9	9.3855
1300	1.4521	4682.5	5408.6	9.7749	1.2101	4682.3	5408.3	9.6906	0.9076	4681.8	5407.9	9.5575

* La temperatura tra parentesi è la temperatura di saturazione a una data pressione.
† Proprietà del vapore saturo a una data pressione.

TABELLA A.6

Acqua surriscaldata (*continua*)

T °C	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)
	p = 1.00 MPa (179.91°C)				p = 1.20 MPa (187.99°C)				p = 1.40 MPa (195.07°C)			
Sat.	0.19444	2583.6	2778.1	6.5865	0.16333	2588.8	2784.8	6.5233	0.14084	2592.8	2790.0	6.4693
200	0.2060	2621.9	2827.9	6.6940	0.16930	2612.8	2815.9	6.5898	0.14302	2603.1	2803.3	6.4975
250	0.2327	2709.9	2942.6	6.9247	0.19234	2704.2	2935.0	6.8294	0.16350	2698.3	2927.2	6.7467
300	0.2579	2793.2	3051.2	7.1229	0.2138	2789.2	3045.8	7.0317	0.18228	2785.2	3040.4	6.9534
350	0.2825	2875.2	3157.7	7.3011	0.2345	2872.2	3153.6	7.2121	0.2003	2869.2	3149.5	7.1360
400	0.3066	2957.3	3263.9	7.4651	0.2548	2954.9	3260.7	7.3774	0.2178	2952.5	3257.5	7.3026
500	0.3541	3124.4	3478.5	7.7622	0.2946	3122.8	3476.3	7.6759	0.2521	3121.1	3474.1	7.6027
600	0.4011	3296.8	3697.9	8.0290	0.3339	3295.6	3696.3	7.9435	0.2860	3294.4	3694.8	7.8710
700	0.4478	3475.3	3923.1	8.2731	0.3729	3474.4	3922.0	8.1881	0.3195	3473.6	3920.8	8.1160
800	0.4943	3660.4	4154.7	8.4996	0.4118	3659.7	4153.8	8.4148	0.3528	3659.0	4153.0	8.3431
900	0.5407	3852.2	4392.9	8.7118	0.4505	3851.6	4392.2	8.6272	0.3861	3851.1	4391.5	8.5556
1000	0.5871	4050.5	4637.6	8.9119	0.4892	4050.0	4637.0	8.8274	0.4192	4049.5	4636.4	8.7559
1100	0.6335	4255.1	4888.6	9.1017	0.5278	4254.6	4888.0	9.0172	0.4524	4254.1	4887.5	8.9457
1200	0.6798	4465.6	5145.4	9.2822	0.5665	4465.1	5144.9	9.1977	0.4855	4464.7	5144.4	9.1262
1300	0.7261	4681.3	5407.4	9.4543	0.6051	4680.9	5407.0	9.3698	0.5186	4680.4	5406.5	9.2984
	p = 1.60 MPa (201.41°C)				p = 1.80 MPa (207.15°C)				p = 2.00 MPa (212.42°C)			
Sat.	0.12380	2596.0	2794.0	6.4218	0.11042	2598.4	2797.1	6.3794	0.09963	2600.3	2799.5	6.3409
225	0.13287	2644.7	2857.3	6.5518	0.11673	2636.6	2846.7	6.4808	0.10377	2628.3	2835.8	6.4147
250	0.14184	2692.3	2919.2	6.6732	0.12497	2686.0	2911.0	6.6066	0.11144	2679.6	2902.5	6.5453
300	0.15862	2781.1	3034.8	6.8844	0.14021	2776.9	3029.2	6.8226	0.12547	2772.6	3023.5	6.7664
350	0.17456	2866.1	3145.4	7.0694	0.15457	2863.0	3141.2	7.0100	0.13857	2859.8	3137.0	6.9563
400	0.19005	2950.1	3254.2	7.2374	0.16847	2947.7	3250.9	7.1794	0.15120	2945.2	3247.6	7.1271
500	0.2203	3119.5	3472.0	7.5390	0.19550	3117.9	3469.8	7.4825	0.17568	3116.2	3467.6	7.4317
600	0.2500	3293.3	3693.2	7.8080	0.2220	3292.1	3691.7	7.7523	0.19960	3290.9	3690.1	7.7024
700	0.2794	3472.7	3919.7	8.0535	0.2482	3471.8	3918.5	7.9983	0.2232	3470.9	3917.4	7.9487
800	0.3086	3658.3	4152.1	8.2808	0.2742	3657.6	4151.2	8.2258	0.2467	3657.0	4150.3	8.1765
900	0.3377	3850.5	4390.8	8.4935	0.3001	3849.9	4390.1	8.4386	0.2700	3849.3	4389.4	8.3895
1000	0.3668	4049.0	4635.8	8.6938	0.3260	4048.5	4635.2	8.6391	0.2933	4048.0	4634.6	8.5901
1100	0.3958	4253.7	4887.0	8.8837	0.3518	4253.2	4886.4	8.8290	0.3166	4252.7	4885.9	8.7800
1200	0.4248	4464.2	5143.9	9.0643	0.3776	4463.7	5143.4	9.0096	0.3398	4463.3	5142.9	8.9607
1300	0.4538	4679.9	5406.0	9.2364	0.4034	4679.5	5405.6	9.1818	0.3631	4679.0	5405.1	9.1329
	p = 2.50 MPa (223.99°C)				p = 3.00 MPa (233.90°C)				p = 3.50 MPa (242.60°C)			
Sat.	0.07998	2603.1	2803.1	6.2575	0.06668	2604.1	2804.2	6.1869	0.05707	2603.7	2803.4	6.1253
225	0.08027	2605.6	2806.3	6.2639								
250	0.08700	2662.6	2880.1	6.4085	0.07058	2644.0	2855.8	6.2872	0.05872	2623.7	2829.2	6.1749
300	0.09890	2761.6	3008.8	6.6438	0.08114	2750.1	2993.5	6.5390	0.06842	2738.0	2977.5	6.4461
350	0.10976	2851.9	3126.3	6.8403	0.09053	2843.7	3115.3	6.7428	0.07678	2835.3	3104.0	6.6579
400	0.12010	2939.1	3239.3	7.0148	0.09936	2932.8	3230.9	6.9212	0.08453	2926.4	3222.3	6.8405
450	0.13014	3025.5	3350.8	7.1746	0.10787	3020.4	3344.0	7.0834	0.09196	3015.3	3337.2	7.0052
500	0.13993	3112.1	3462.1	7.3234	0.11619	3108.0	3456.5	7.2338	0.09918	3103.0	3450.9	7.1572
600	0.15930	3288.0	3686.3	7.5960	0.13243	3285.0	3682.3	7.5085	0.11324	3282.1	3678.4	7.4339
700	0.17832	3468.7	3914.5	7.8435	0.14838	3466.5	3911.7	7.7571	0.12699	3464.3	3908.8	7.6837
800	0.19716	3655.3	4148.2	8.0720	0.16414	3653.5	4145.9	7.9862	0.14056	3651.8	4143.7	7.9134
900	0.21590	3847.9	4387.6	8.2853	0.17980	3846.5	4385.9	8.1999	0.15402	3845.0	4384.1	8.1276
1000	0.2346	4046.7	4633.1	8.4861	0.19541	4045.4	4631.6	8.4009	0.16743	4044.1	4630.1	8.3288
1100	0.2532	4251.5	4884.6	8.6762	0.21098	4250.3	4883.3	8.5912	0.18080	4249.2	4881.9	8.5192
1200	0.2718	4462.1	5141.7	8.8569	0.22652	4460.9	5140.5	8.7720	0.19415	4459.8	5139.3	8.7000
1300	0.2905	4677.8	5404.0	9.0291	0.24206	4676.6	5402.8	8.9442	0.20749	4675.5	5401.7	8.8723

TABELLA A.6
Acqua surriscaldata (*continua*)

T °C	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)
	p = 4.0 MPa (250.40°C)				p = 4.5 MPa (257.49°C)				p = 5.0 MPa (263.99°C)			
Sat.	0.04978	2602.3	2801.4	6.0701	0.04406	2600.1	2798.3	6.0198	0.03944	2597.1	2794.3	5.9734
275	0.05457	2667.9	2886.2	6.2285	0.04730	2650.3	2863.2	6.1401	0.04141	2631.3	2838.3	6.0544
300	0.05884	2725.3	2960.7	6.3615	0.05135	2712.0	2943.1	6.2828	0.04532	2698.0	2924.5	6.2084
350	0.06645	2826.7	3092.5	6.5821	0.05840	2817.8	3080.6	6.5131	0.05194	2808.7	3068.4	6.4493
400	0.07341	2919.9	3213.6	6.7690	0.06475	2913.3	3204.7	6.7047	0.05781	2906.6	3195.7	6.6459
450	0.08002	3010.2	3330.3	6.9363	0.07074	3005.0	3323.3	6.8746	0.06330	2999.7	3316.2	6.8186
500	0.08643	3099.5	3445.3	7.0901	0.07651	3095.3	3439.6	7.0301	0.06857	3091.0	3433.8	6.9759
600	0.09885	3279.1	3674.4	7.3688	0.08765	3276.0	3670.5	7.3110	0.07869	3273.0	3666.5	7.2589
700	0.11095	3462.1	3905.9	7.6198	0.09847	3459.9	3903.0	7.5631	0.08849	3457.6	3900.1	7.5122
800	0.12287	3650.0	4141.5	7.8502	0.10911	3648.3	4139.3	7.7942	0.09811	3646.6	4137.1	7.7440
900	0.13469	3843.6	4382.3	8.0647	0.11965	3842.2	4380.6	8.0091	0.10762	3840.7	4378.8	7.9593
1000	0.14645	4042.9	4628.7	8.2662	0.13013	4041.6	4627.2	8.2108	0.11707	4040.4	4625.7	8.1612
1100	0.15817	4248.0	4880.6	8.4567	0.14056	4246.8	4879.3	8.4015	0.12648	4245.6	4878.0	8.3520
1200	0.16987	4458.6	5138.1	8.6376	0.15098	4457.5	5136.9	8.5825	0.13587	4456.3	5135.7	8.5331
1300	0.18156	4674.3	5400.5	8.8100	0.16139	4673.1	5399.4	8.7549	0.14526	4672.0	5398.2	8.7055
	p = 6.0 MPa (275.64°C)				p = 7.0 MPa (285.88°C)				p = 8.0 MPa (295.06°C)			
Sat.	0.03244	2589.7	2784.3	5.8892	0.02737	2580.5	2772.1	5.8133	0.02352	2569.8	2758.0	5.7432
300	0.03616	2667.2	2884.2	6.0674	0.02947	2632.2	2838.4	5.9305	0.02426	2590.9	2785.0	5.7906
350	0.04223	2789.6	3043.0	6.3335	0.03524	2769.4	3016.0	6.2283	0.02995	2747.7	2987.3	6.1301
400	0.04739	2892.9	3177.2	6.5408	0.03993	2878.6	3158.1	6.4478	0.03432	2863.8	3138.3	6.3634
450	0.05214	2988.9	3301.8	6.7193	0.04416	2978.0	3287.1	6.6327	0.03817	2966.7	3272.0	6.5551
500	0.05665	3082.2	3422.2	6.8803	0.04814	3073.4	3410.3	6.7975	0.04175	3064.3	3398.3	6.7240
550	0.06101	3174.6	3540.6	7.0288	0.05195	3167.2	3530.9	6.9486	0.04516	3159.8	3521.0	6.8778
600	0.06525	3266.9	3658.4	7.1677	0.05565	3260.7	3650.3	7.0894	0.04845	3254.4	3642.0	7.0206
700	0.07352	3453.1	3894.2	7.4234	0.06283	3448.5	3888.3	7.3476	0.05481	3443.9	3882.4	7.2812
800	0.08160	3643.1	4132.7	7.6566	0.06981	3639.5	4128.2	7.5822	0.06097	3636.0	4123.8	7.5173
900	0.08958	3837.8	4375.3	7.8727	0.07669	3835.0	4371.8	7.7991	0.06702	3832.1	4368.3	7.7351
1000	0.09749	4037.8	4622.7	8.0751	0.08350	4035.3	4619.8	8.0020	0.07301	4032.8	4616.9	7.9384
1100	0.10536	4243.3	4875.4	8.2661	0.09027	4240.9	4872.8	8.1933	0.07896	4238.6	4870.3	8.1300
1200	0.11321	4454.0	5133.3	8.4474	0.09703	4451.7	5130.9	8.3747	0.08489	4449.5	5128.5	8.3115
1300	0.12106	4669.6	5396.0	8.6199	0.10377	4667.3	5393.7	8.5475	0.09080	4665.0	5391.5	8.4842
	p = 9.0 MPa (303.40°C)				p = 10.0 MPa (311.06°C)				p = 12.5 MPa (327.89°C)			
Sat.	0.02048	2557.8	2742.1	5.6772	0.018026	2544.4	2724.7	5.6141	0.013495	2505.1	2673.8	5.4624
325	0.02327	2646.6	2856.0	5.8712	0.019861	2610.4	2809.1	5.7568				
350	0.02580	2724.4	2956.6	6.0361	0.02242	2699.2	2923.4	5.9443	0.016126	2624.6	2826.2	5.7118
400	0.02993	2848.4	3117.8	6.2854	0.02641	2832.4	3096.5	6.2120	0.02000	2789.3	3039.3	6.0417
450	0.03350	2955.2	3256.6	6.4844	0.02975	2943.4	3240.9	6.4190	0.02299	2912.5	3199.8	6.2719
500	0.03677	3055.2	3386.1	6.6576	0.03279	3045.8	3373.7	6.5966	0.02560	3021.7	3341.8	6.4618
550	0.03987	3152.2	3511.0	6.8142	0.03564	3144.6	3500.9	6.7561	0.02801	3125.0	3475.2	6.6290
600	0.04285	3248.1	3633.7	6.9589	0.03837	3241.7	3625.3	6.9029	0.03029	3225.4	3604.0	6.7810
650	0.04574	3343.6	3755.3	7.0943	0.04101	3338.2	3748.2	7.0398	0.03248	3324.4	3730.4	6.9218
700	0.04857	3439.3	3876.5	7.2221	0.04358	3434.7	3870.5	7.1687	0.03460	3422.9	3855.3	7.0536
800	0.05409	3632.5	4119.3	7.4596	0.04859	3628.9	4114.8	7.4077	0.03869	3620.0	4103.6	7.2965
900	0.05950	3829.2	4364.8	7.6783	0.05349	3826.3	4361.2	7.6272	0.04267	3819.1	4352.5	7.5182
1000	0.06485	4030.3	4614.0	7.8821	0.05832	4027.8	4611.0	7.8315	0.04658	4021.6	4603.8	7.7237
1100	0.07016	4236.3	4867.7	8.0740	0.06312	4234.0	4865.1	8.0237	0.05045	4228.2	4858.8	7.9165
1200	0.07544	4447.2	5126.2	8.2556	0.06789	4444.9	5123.8	8.2055	0.05430	4439.3	5118.0	8.0937
1300	0.08072	4662.7	5389.2	8.4284	0.07265	4460.5	5387.0	8.3783	0.05813	4654.8	5381.4	8.2717

TABELLA A.6

Acqua surriscaldata (*continua*)

T °C	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg · K)
	p = 15.0 MPa (342.24°C)				p = 17.5 MPa (354.75°C)				p = 20.0 MPa (365.81°C)			
Sat.	0.010337	2455.5	2610.5	5.3098	0.007920	2390.2	2528.8	5.1419	0.005834	2293.0	2409.7	4.9269
350	0.011470	2520.4	2692.4	5.4421								
400	0.015649	2740.7	2975.5	5.8811	0.012447	2685.0	2902.9	5.7213	0.009942	2619.3	2818.1	5.5540
450	0.018445	2879.5	3156.2	6.1404	0.015174	2844.2	3109.7	6.0184	0.012695	2806.2	3060.1	5.9017
500	0.02080	2996.6	3308.6	6.3443	0.017358	2970.3	3274.1	6.2383	0.014768	2942.9	3238.2	6.1401
550	0.02293	3104.7	3448.6	6.5199	0.019288	3083.9	3421.4	6.4230	0.016555	3062.4	3393.5	6.3348
600	0.02491	3208.6	3582.3	6.6776	0.02106	3191.5	3560.1	6.5866	0.018178	3174.0	3537.6	6.5048
650	0.02680	3310.3	3712.3	6.8224	0.02274	3296.0	3693.9	6.7357	0.019693	3281.4	3675.3	6.6582
700	0.02861	3410.9	3840.1	6.9572	0.02434	3398.7	3824.6	6.8736	0.02113	3386.4	3809.0	6.7993
800	0.03210	3610.9	4092.4	7.2040	0.02738	3601.8	4081.1	7.1244	0.02385	3592.7	4069.7	7.0544
900	0.03546	3811.9	4343.8	7.4279	0.03031	3804.7	4335.1	7.3507	0.02645	3797.5	4326.4	7.2830
1000	0.03875	4015.4	4596.6	7.6348	0.03316	4009.3	4589.5	7.5589	0.02897	4003.1	4582.5	7.4925
1100	0.04200	4222.6	4852.6	7.8283	0.03597	4216.9	4846.4	7.7531	0.03145	4211.3	4840.2	7.6874
1200	0.04523	4433.8	5112.3	8.0108	0.03876	4428.3	5106.6	7.9360	0.03391	4422.8	5101.0	7.8707
1300	0.04845	4649.1	5376.0	8.1840	0.04154	4643.5	5370.5	8.1093	0.03636	4638.0	5365.1	8.0442
	p = 25.0 MPa				p = 30.0 MPa				p = 35.0 MPa			
375	0.0019731	1798.7	1848.0	4.0320	0.0017892	1737.8	1791.5	3.9305	0.0017003	1702.9	1762.4	3.8722
400	0.006004	2430.1	2580.2	5.1418	0.002790	2067.4	2151.1	4.4728	0.002100	1914.1	1987.6	4.2126
425	0.007881	2609.2	2806.3	5.4723	0.005303	2455.1	2614.2	5.1504	0.003426	2253.4	2373.4	4.7747
450	0.009162	2720.7	2949.7	5.6744	0.006735	2619.3	2821.4	5.4424	0.004961	2498.7	2672.4	5.1962
500	0.011123	2884.3	3162.4	5.9592	0.008678	2820.7	3081.1	5.7905	0.006927	2751.9	2994.4	5.6282
550	0.012724	3017.5	3335.6	6.1765	0.010168	2970.3	3275.4	6.0342	0.008345	2921.0	3213.0	5.9026
600	0.014137	3137.9	3491.4	6.3602	0.011446	3100.5	3443.9	6.2331	0.009527	3062.0	3395.5	6.1179
650	0.015433	3251.6	3637.4	6.5229	0.012596	3221.0	3598.9	6.4058	0.010575	3189.8	3559.9	6.3010
700	0.016646	3361.3	3777.5	6.6707	0.013661	3335.8	3745.6	6.5606	0.011533	3309.8	3713.5	6.4631
800	0.018912	3574.3	4047.1	6.9345	0.015623	3555.5	4024.2	6.8332	0.013278	3536.7	4001.5	6.7450
900	0.021045	3783.0	4309.1	7.1680	0.017448	3768.5	4291.9	7.0718	0.014883	3754.0	4274.9	6.9386
1000	0.02310	3990.9	4568.5	7.3802	0.019196	3978.8	4554.7	7.2867	0.016410	3966.7	4541.1	7.2064
1100	0.02512	4200.2	4828.2	7.5765	0.020903	4189.2	4816.3	7.4845	0.017895	4178.3	4804.6	7.4037
1200	0.02711	4412.0	5089.9	7.7605	0.022589	4401.3	5079.0	7.6692	0.019360	4390.7	5068.3	7.5910
1300	0.02910	4626.9	5354.4	7.9342	0.024266	4616.0	5344.0	7.8432	0.020815	4605.1	5333.6	7.7653
	p = 40.0 MPa				p = 50.0 MPa				p = 60.0 MPa			
375	0.0016407	1677.1	1742.8	3.8290	0.0015594	1638.6	1716.6	3.7639	0.0015028	1609.4	1699.5	3.7141
400	0.0019077	1854.6	1930.9	4.1135	0.0017309	1788.1	1874.6	4.0031	0.0016335	1745.4	1843.4	3.9318
425	0.002532	2096.9	2198.1	4.5029	0.002007	1959.7	2060.0	4.2734	0.0018165	1892.7	2001.7	4.1626
450	0.003693	2365.1	2512.8	4.9459	0.002486	2159.6	2284.0	4.5884	0.002085	2053.9	2179.0	4.4121
500	0.005622	2678.4	2903.3	5.4700	0.003892	2525.5	2720.1	5.1726	0.002956	2390.6	2567.9	4.9321
550	0.006984	2869.7	3149.1	5.7785	0.005118	2763.6	3019.5	5.5485	0.003956	2658.8	2896.2	5.3441
600	0.008094	3022.6	3346.4	6.0144	0.006112	2942.0	3247.6	5.8178	0.004834	2861.1	3151.2	5.6452
650	0.009063	3158.0	3520.6	6.2054	0.006966	3093.5	3441.8	6.0342	0.005595	3028.8	3364.5	5.8829
700	0.009941	3283.6	3681.2	6.3750	0.007727	3230.5	3616.8	6.2189	0.006272	3177.2	3553.5	6.0824
800	0.011523	3517.8	3978.7	6.6662	0.009076	3479.8	3933.6	6.5290	0.007459	3441.5	3889.1	6.4109
900	0.012962	3739.4	4257.9	6.9150	0.010283	3710.3	4224.4	6.7882	0.008508	3681.0	4191.5	6.6805
1000	0.014324	3954.6	4527.6	7.1356	0.011411	3930.5	4501.1	7.0146	0.009480	3906.4	4475.2	6.9127
1100	0.015642	4167.4	4793.1	7.3364	0.012496	4145.7	4770.5	7.2184	0.010409	4124.1	4748.6	7.1195
1200	0.016940	4380.1	5057.7	7.5224	0.013561	4359.1	5037.2	7.4058	0.011317	4338.2	5017.2	7.3083
1300	0.018229	4594.3	5323.5	7.6969	0.014616	4572.8	5303.6	7.5808	0.012215	4551.4	5284.3	7.4837

Regola della leva

proprietà *Valida all'interno della campana → condizioni di saturazione*

v, h, s, u → sono grandezze estensive, proporzionali alla massa.

V_{ls} → liquido saturo

V_{vs} → vapore saturo

m_v → massa del gas

m_l → massa del liquido

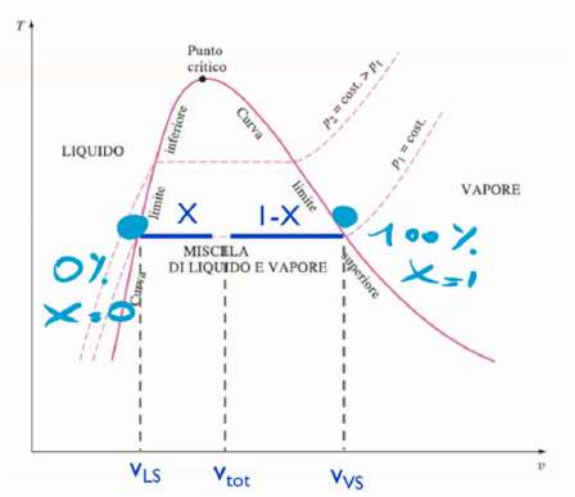
$$m_{tot} = m_v + m_l$$

Titolo di vapore (frazione di gas)

$$X = \frac{m_v}{m_{tot}} \rightarrow \text{grandezza percentuale}[\%]$$

Frazione di liquido

$$1 - X = \frac{m_l}{m_{tot}} \rightarrow \text{grandezza percentuale}[\%]$$



Calcolo V → processo analogo anche per H, S, U

$H = h \cdot m \qquad S = s \cdot m \qquad U = u \cdot m \qquad V = v \cdot m$

$$V_{tot} = V_{ls} + V_{vs} = m_l \cdot v_{ls} + m_v \cdot v_{vs} \qquad [m^3]$$

v_{ls}, v_{vs}, come anche h_{vs}, s_{vs}, u_{vs} e h_{ls}, s_{ls}, u_{ls} sono valutati agli estremi della campana (ls, vs) con le tabelle sopra mostrate.

OPPURE:

$$\underset{\text{volume specifico}}{v_{tot}} = (1 - X) \cdot v_{ls} + X \cdot v_{vs} \qquad \left[\frac{m^3}{Kg}\right]$$

$$V_{tot} = m_{tot} \cdot v_{tot} \qquad [m^3]$$

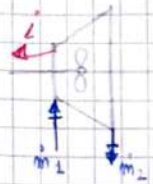
Esempi esercizi sui liquidi

▼ Esempio esercizio miscela liquido+vapore

https://s3-us-west-2.amazonaws.com/secure.notion-static.com/db80291f-215d-49b2-80e6-8064fca6a083/Esercizio_liquido.pdf

▼ Esempio turbina a vapore ideale adiabatica (sistema aperto)

Esercizio 2 → TURBINA IDEALE → [illegible] TURBINA a VAPORE



Ideale → $Q = 0$, TIR

$\dot{L}$ → potenza meccanica

$\dot{m}_1 = \dot{m}_2$ (non varia la portata massica → no Termini d'accumulo)

$\dot{m}_1 = \dot{m}_2 = 150\ kg/s$ di vapor d'acqua

$P_1 = 175\ bar = 17{,}5\ MPa$ $\quad T_1 = 650\ °C = 923{,}15\ K$

$P_2 = 20\ kPa$

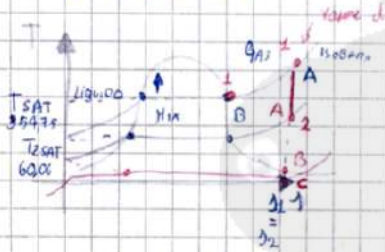
? $\dot{L}$, T_2, X_2 (Titolo di VAPORE)

TURBINA:
- APERTO
- IDEALE • $Q = 0$ • TIR } isoentropica → $s_1 = s_2$

Vapore ≠ GAS IDEALE (usiamo la Tabella)

BILANCIO ENERGIA → 1° PRINCIPIO

$$\dot{m}_1 h_1 - \dot{L} - \dot{m}_2 h_2 = 0 \qquad \dot{L} = \dot{m}(h_1 - h_2)$$



ISOBARA è data isoterma nella campana

A: Vapore Surriscaldato
$T_2 > T_{SAT}$

B: Vapore saturo
$T_1 = T_{SAT}$

$T_{SAT} = 354{,}75\ °C$ (Tabelle)
$T_1 = 650\ °C$
$T_1 > T_{SAT}$ → Vapore surriscaldato

$h_1 = h_{vap\ surr}(P_1, T_1) = 3693{,}9\ \frac{kJ}{kg}$ (Tabella)

$s_1 = s_{vap\ surr}(P_1, T_1) = 6{,}7357\ \frac{kJ}{kgK}$ (Tabella)

A: se $s_2 > s_{VSAT}(20\ kPa) = s_2$

B: $s_2 = s_{VSAT}$

C: se $s_2 < s_{VS}$ (dentro la campana)

Isoentropica ≠ politropica (non posso calcolare le cadute)

$s_2 = s_1$ $(P_2 = 20\ kPa)$

$s_{VSAT} = 7{,}9085$ $\quad s_2 = s_1 = 6{,}7357$
$s_{LSAT} = 0{,}8320$

$h_{VSAT} = 2906$
$h_{LS} = 251{,}04$

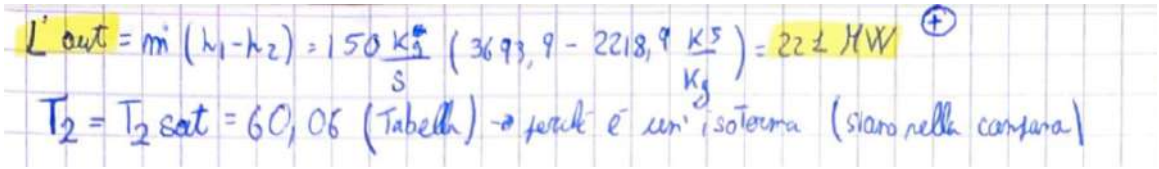
Regola della leva $\boxed{s_2 = s_{LS}(1 - x_2) + s_{VS}(x_2)}$

$s_2 < s_{VSAT}$ → Condizione C, siamo dentro la campana

$$x_2 = \frac{s_2 - s_{LS}}{s_{VS} - s_{LS}} = 0{,}834 \quad (83\%\ \text{vapore})$$

Siamo già vicini alle Caldaie di vapore saturo

$$h_2 = h_{LS}\cdot(1 - x_2) + h_{VS}(x_2) \rightarrow 2218{,}9\ \frac{kJ}{kg}$$



▼ Esempio trasformazione isobara (sistema aperto) → scambiatore di calore liquido + gas